

# Intensifikasi Proses Produksi $H_2$ sebagai Energi Bersih Masa Depan

Air sebagai bahan bakar. Mungkinkah?

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# Intensifikasi Proses

- Emerging equipment, processing techniques, and operational methods promise spectacular improvements in process plants, markedly shrinking their size and dramatically boosting their efficiency. These developments may result in the extinction of some traditional types of equipment, if not whole unit operations (**Stankiewicz and Moulijn, 2000**).
- Apa yang dimaksud dengan Intensifikasi Proses?
- New paradigm shift in chemical processes
- Kemaslahatan intensifikasi proses



Moulijn



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Stankiewicz

# Intensifikasi Proses

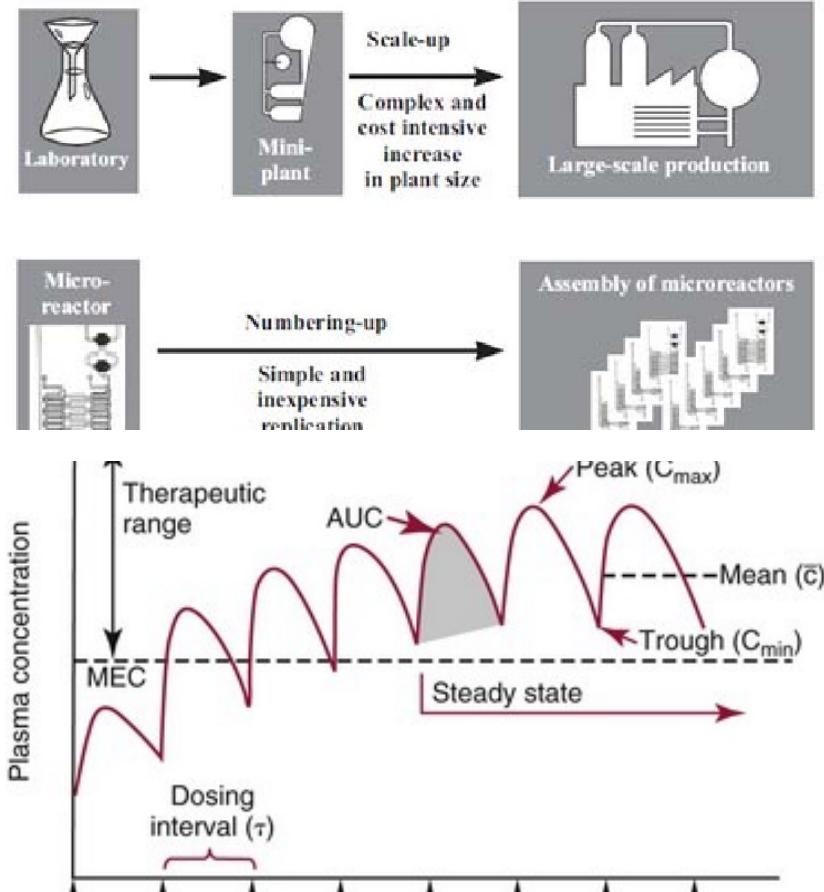
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Pengembangan **peralatan** dan **metode** proses dan sistem pemroses + **material** yang **inovatif** dan **kreatif**

Kinerja meningkat ribuan kali

## New paradigm shift:

- Scale up versus Scale out atau numbering up (Macroscale versus Microscale; Longer versus shorter time to market)
- Steady state versus Unsteady state



## Benefits of process intensification

### Business:

- Miniaturized plant size.
- Reduced CAPEX and OPEX.
- Distributed manufacturing.
- Faster transformation from research to market.

### Process:

- Higher selectivity/product purity.
- Higher reaction rates.
- Improved product properties.
- Improved process safety.
- Wider processing conditions.
- Continuous processing.

### Environment:

- Reduced energy usage.
- Reduced wastage.
- Reduced solvent usage.
- Smaller plants equal to less obstruction on landscape.

Responsive processing

Faster, safer, and greener processing

Sustainable processing



Bagaimana implementasi dari intensifikasi proses dalam proses produksi hidrogen?

Pengembangan **peralatan, metode + material** yang inovatif dan kreatif

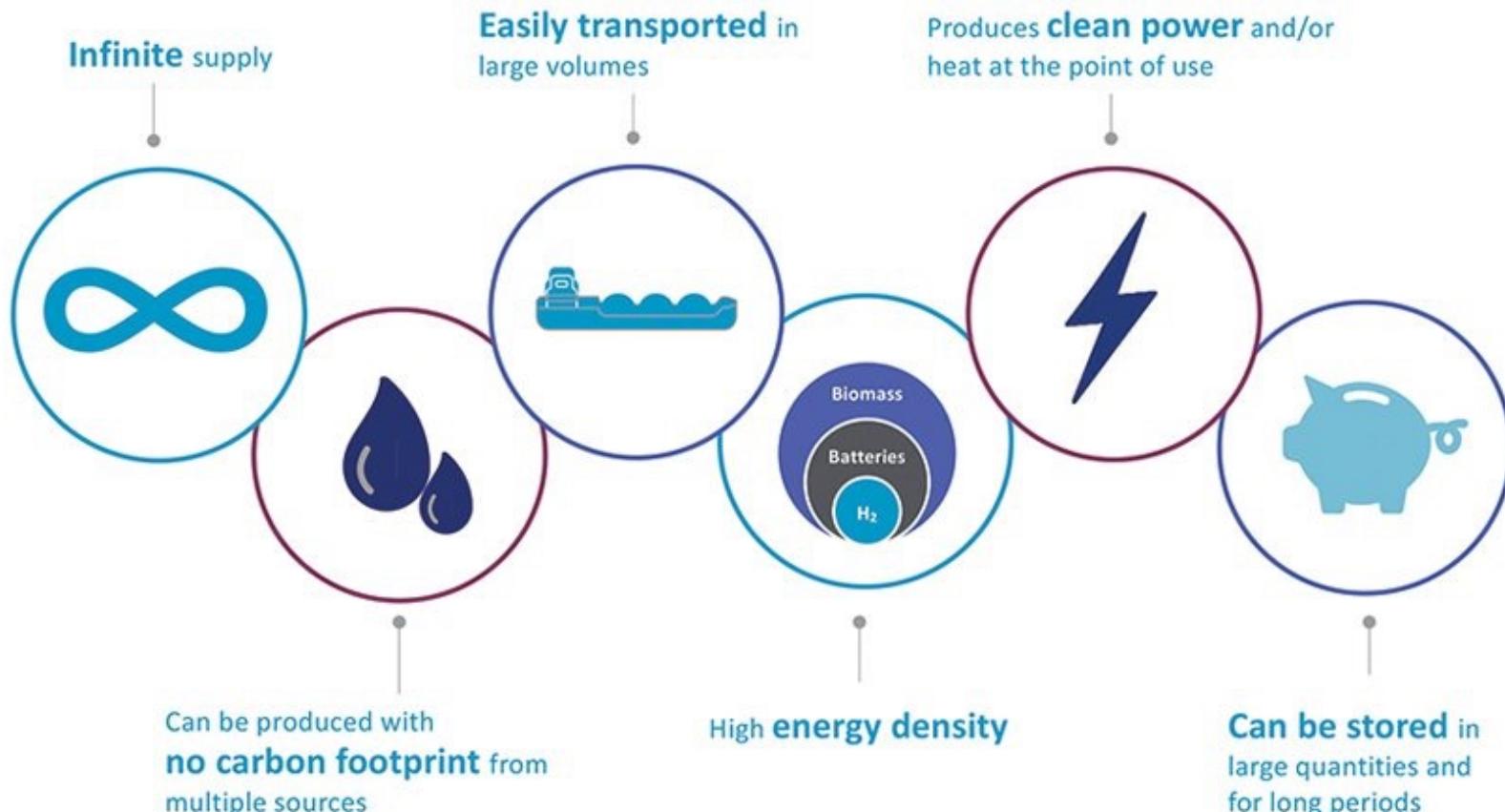


# Mengapa H<sub>2</sub>?

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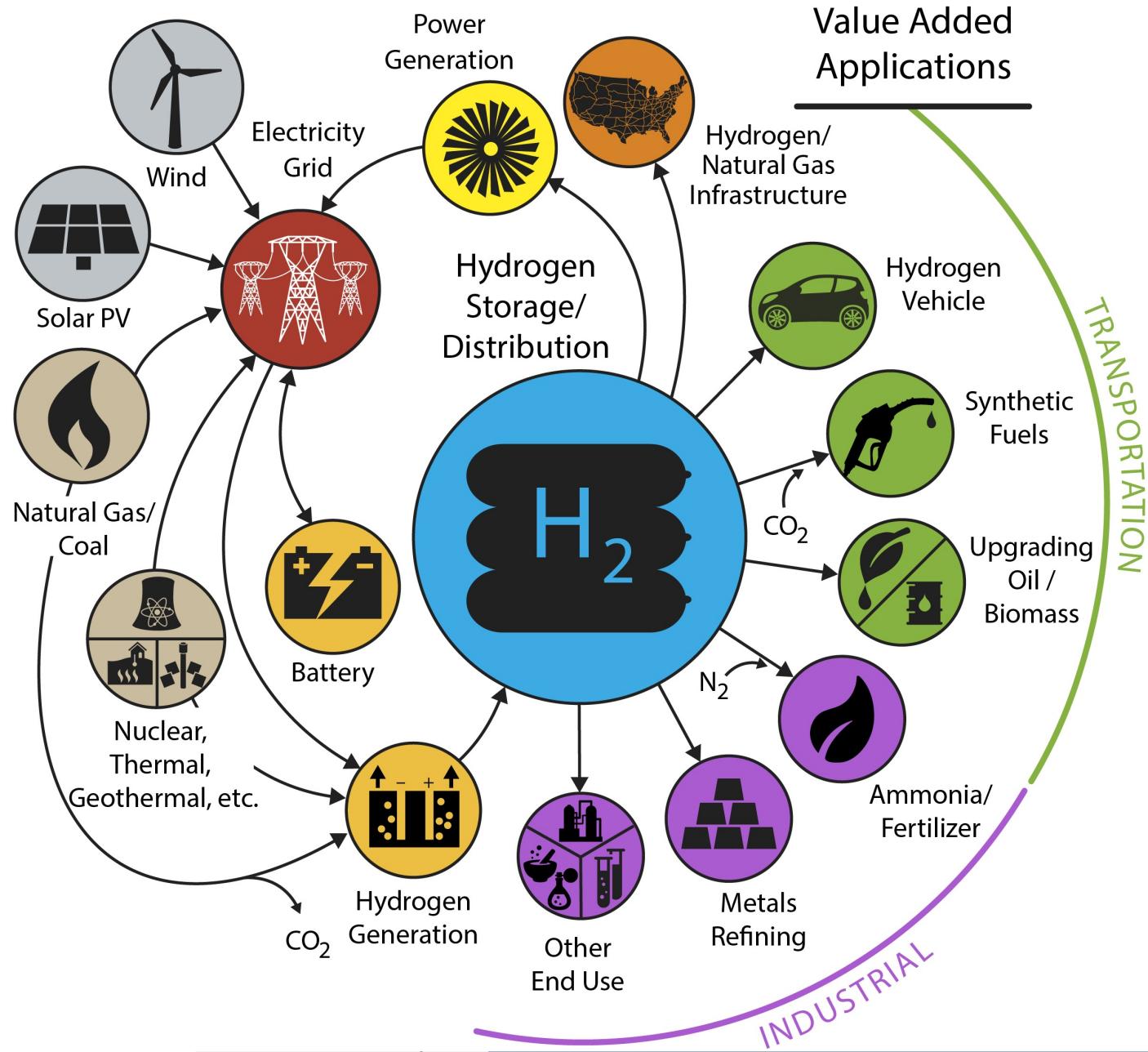
## Why hydrogen?

A versatile, zero-emission, efficient energy carrier



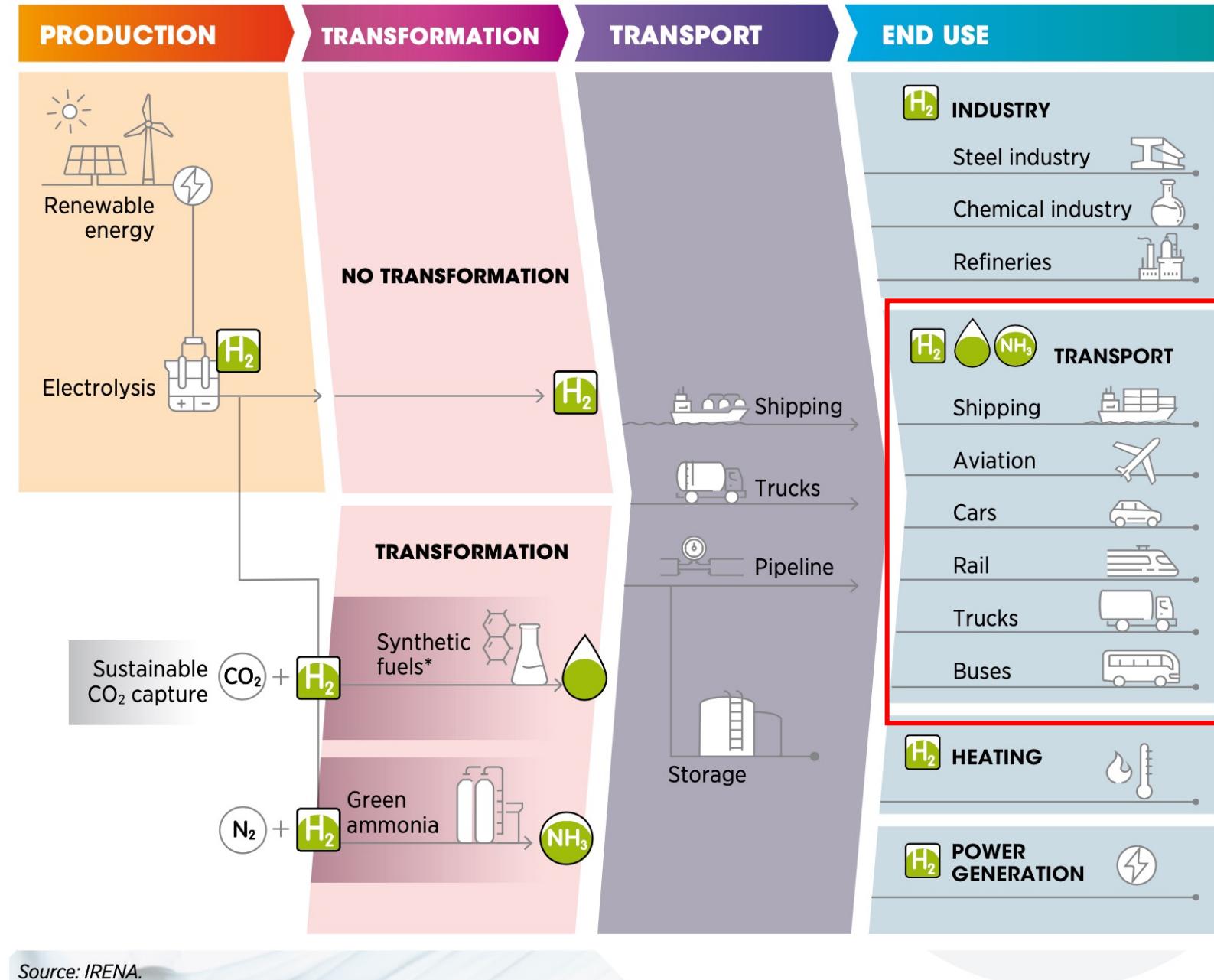
# Aplikasi Nilai Tambah

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# Bagaimana H<sub>2</sub> memberdayakan transisi energi?

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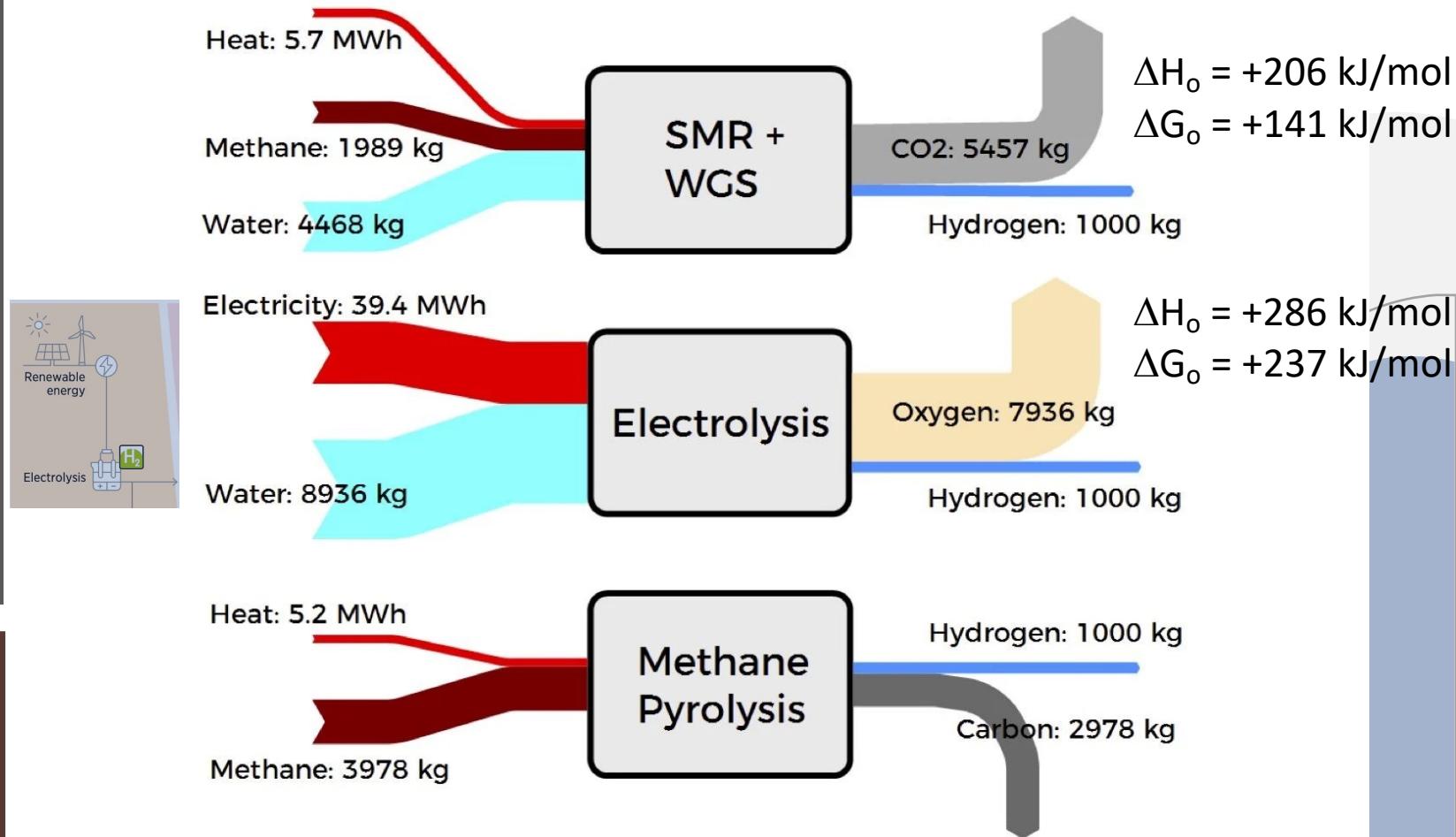
# Berapa Besar Energi yang Diperlukan?

Kelayakan ekonomi  
elektrolisis air dapat diuji  
dengan ketersediaan  
energi yang bersifat  
ekses (**renewable**)

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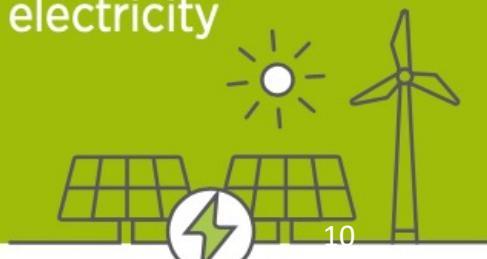
## HYDROGEN PRODUCTION PATHWAYS

(at 100% efficiency)



Kelayakan secara ekonomi, dampak lingkungan (termasuk sumber listrik yang digunakan), keselamatan proses

# Spektrum Warna H<sub>2</sub>

Color	GREY HYDROGEN	BLUE HYDROGEN	TURQUOISE HYDROGEN*	GREEN HYDROGEN
Process	SMR or gasification	SMR or gasification with carbon capture (85-95%)	Pyrolysis	Electrolysis
Source	Methane or coal 	Methane or coal 	Methane 	Renewable electricity 

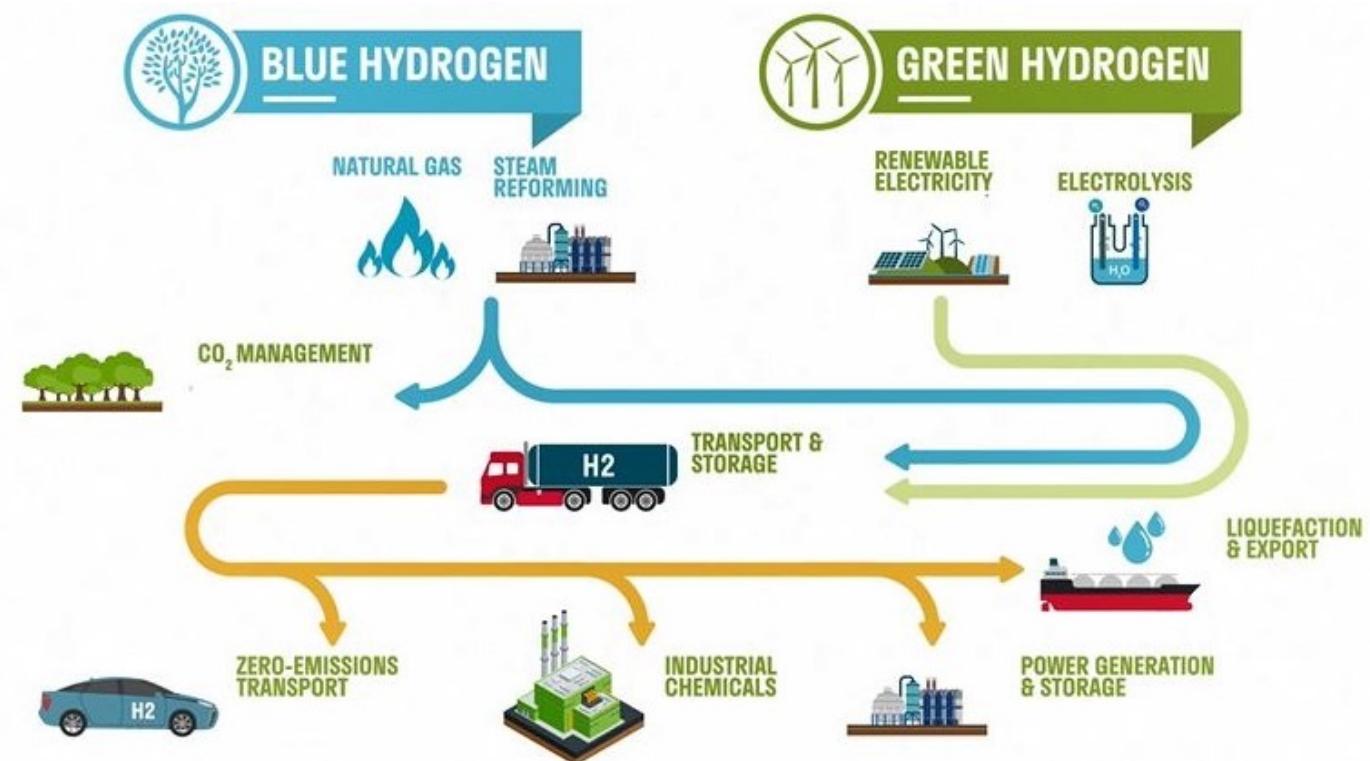
# Spektrum Warna H<sub>2</sub>

## The Hydrogen Colour Spectrum

Colours are used to denote the production method through which hydrogen is obtained

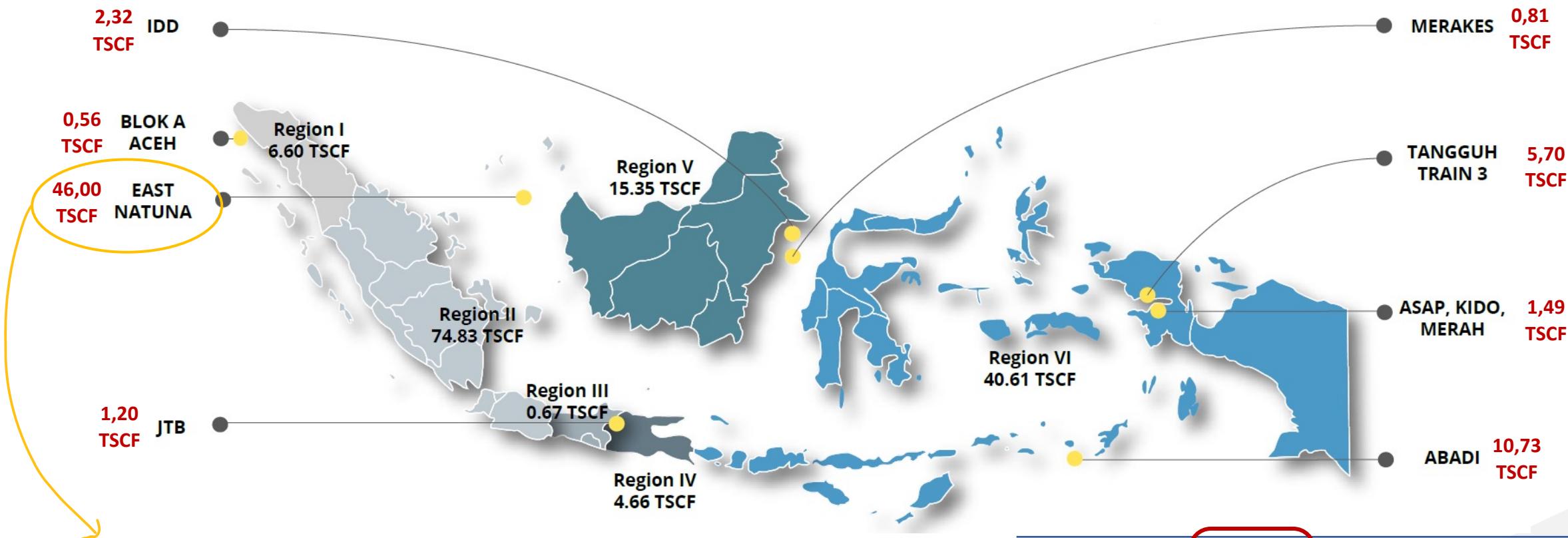


- Saat ini mayoritas H<sub>2</sub> dihasilkan dari gas alam (CO<sub>2</sub> lebih kecil) atau batubara (CO<sub>2</sub> lebih besar): **grey and blue hydrogen**



# Cadangan Gas Alam di Indonesia: Grey dan Blue H<sub>2</sub>

(Sumber: Ditjen Migas dan SKK Migas, 2018)



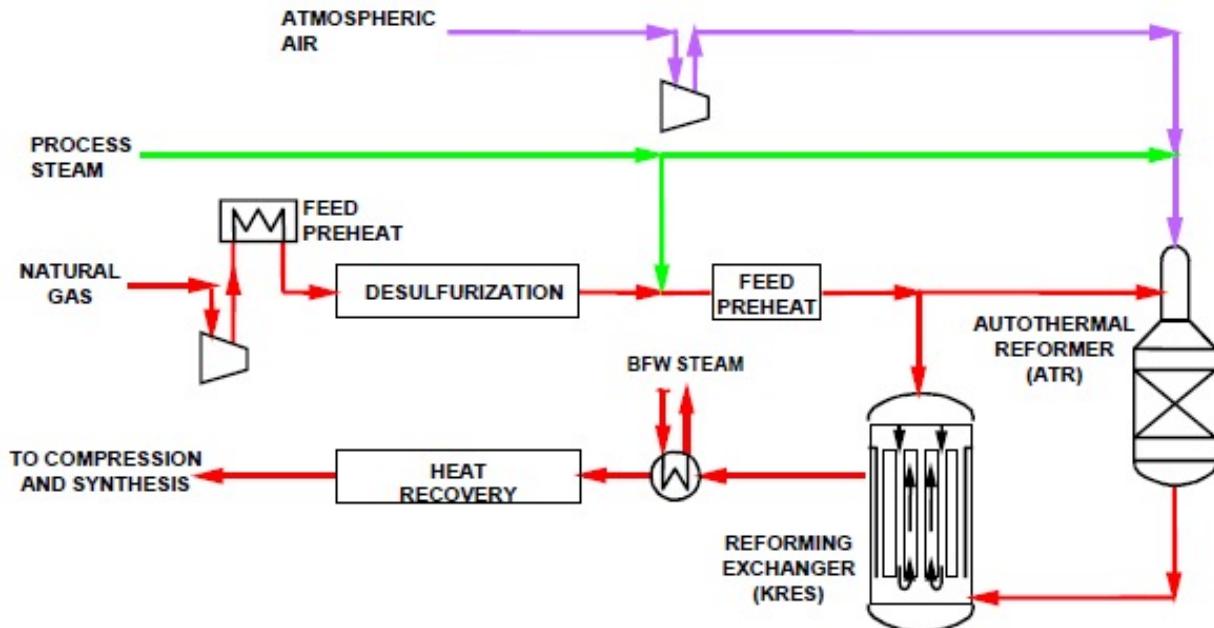
**Kepulauan Natuna → cadangan gas bumi terbesar di Indonesia (46 TSCF).**

Komposisi CO<sub>2</sub> sangat tinggi sehingga pemanfaatannya masih terhambat.

Komponen	Natuna Timur	Bontang	JTB
CH <sub>4</sub>	28-%v	90%	-
CO <sub>2</sub>	71-%v	5%	34%
C <sub>2+</sub> , H <sub>2</sub> S	1-%v	5%	-

# Periodisasi Teknologi Reformasi

- Teknologi **steam reforming** gas alam ( $\text{CO}_2 < 10\%$ , separated)
  - Konvensional > 50 tahun
  - Termodifikasi **Kellogg Reforming Exchanger System** (less energy, less pollution)  $\pm 30$  tahun
- Teknologi **dry reforming** gas alam ( $\text{CO}_2 > 70\%$ , separated)
  - Natuna dan Aceh
  - *Linde Pilot Dry Reformer* di Pullach, Munich, Jerman
- ITB: Katalis berbasis **Ni** memiliki konversi  $\text{CH}_4$  per massa pusat aktif mencapai **2,5 kali lipat lebih tinggi dibandingkan katalis steam reforming komersial**
- ITB: Tri-Reforming (SMR, DRM, PO)



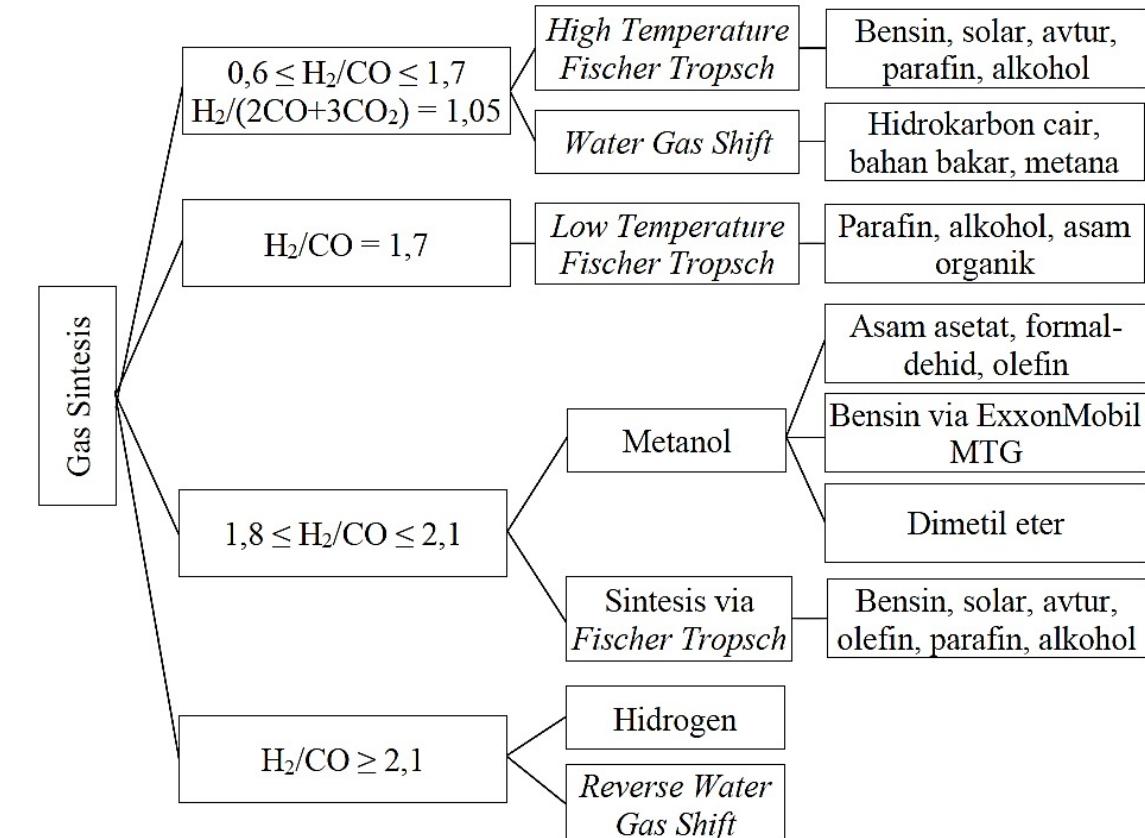
Kellogg Braun & Root (KBR)

# Jenis Reformasi Metana: Grey Hydrogen

Tipe reformasi metana	Dry reforming	Steam reforming	Partial oxidation
Kondisi operasi	1 atm, 650-850°C CH <sub>4</sub> : CO <sub>2</sub> = 1 : 1	3-5 atm, 700-1.000°C CH <sub>4</sub> : H <sub>2</sub> O = 1:1	100 atm, 950-1.100°C CH <sub>4</sub> : O <sub>2</sub> = 2 : 1
Rasio H <sub>2</sub> /CO	1 : 1	3 : 1	2 : 1
Keuntungan	<ul style="list-style-type: none"> <li>- Utilisasi 2 gas rumah kaca</li> <li>- Produksi sumber energi bersih dan bahan kimia lain</li> </ul>	<ul style="list-style-type: none"> <li>- Konsentrasi produk H<sub>2</sub> lebih tinggi</li> <li>- Efisiensi operasi tinggi</li> </ul>	<ul style="list-style-type: none"> <li>- Tingkat toleran terhadap sulfur tinggi</li> <li>- Waktu kontak (reaksi) singkat</li> </ul>
Kerugian	<ul style="list-style-type: none"> <li>- Harga katalis logam mulia yang tinggi</li> <li>- Katalis tersintering pada temperatur tinggi</li> </ul>	<ul style="list-style-type: none"> <li>- Memerlukan volume yang besar untuk emisi gas dari pembangkit uap</li> <li>- Biaya tambahan dari alat eksternal untuk penukar panas</li> </ul>	<ul style="list-style-type: none"> <li>- Biaya tinggi untuk kebutuhan O<sub>2</sub> murni</li> <li>- Kemungkinan ledakan dari campuran CH<sub>4</sub>/O<sub>2</sub></li> <li>- Kemungkinan terjadinya hotspot pada katalis</li> </ul>
Pabrik	Linde Pilot Dry Reformer di Pullach dekat Munich	<ul style="list-style-type: none"> <li>- Topsoe Package H<sub>2</sub> Plants, USA</li> <li>- Air Liquid Steam CH<sub>4</sub> Reformer, Jerman</li> </ul>	Pearl GTL, Ras Laffan Industrial City, Ad-Dahirah, Qatar

(Sumber: Abdulsheeh dkk., 2019)

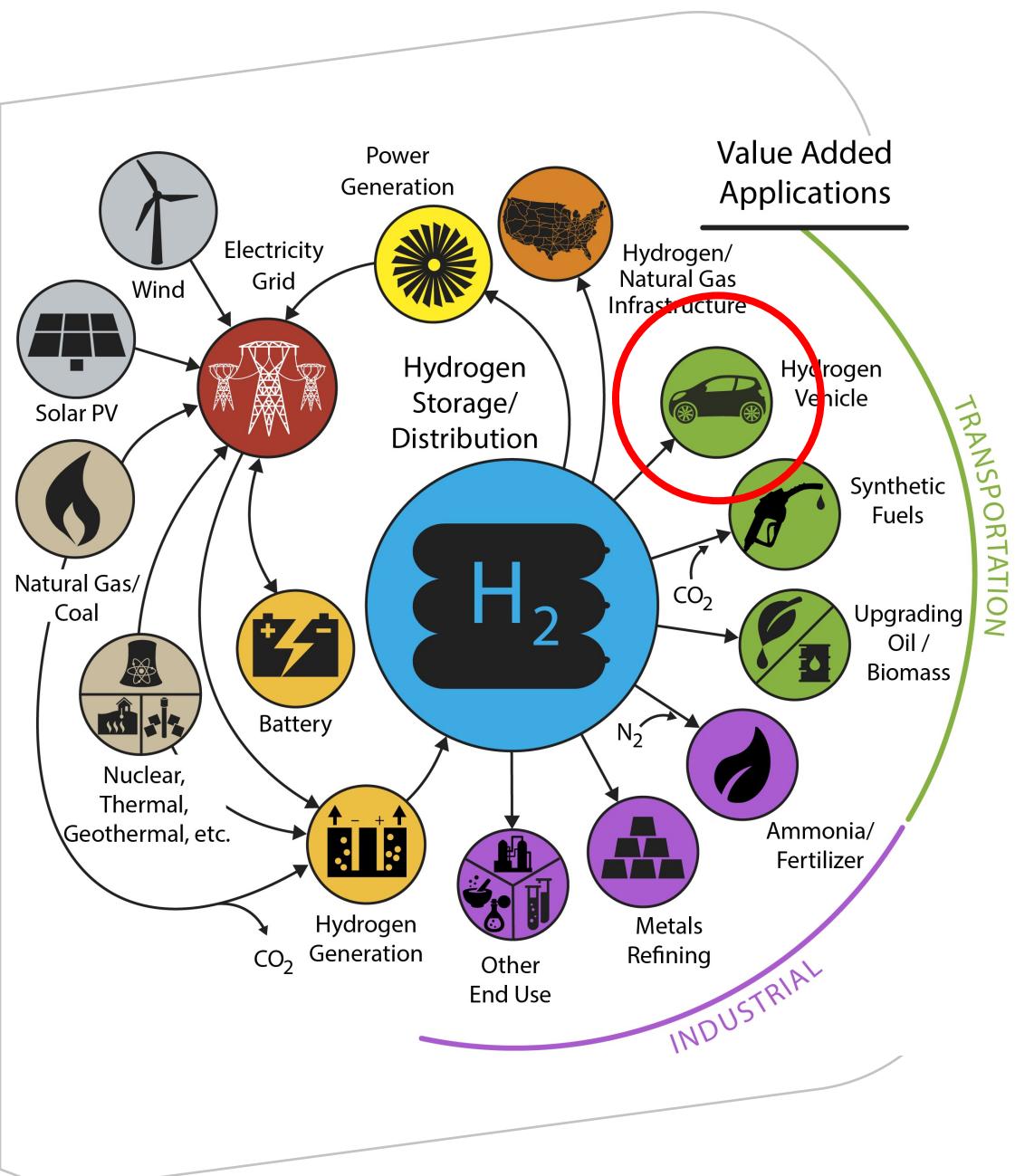
## Rute konversi gas sintesis



No.	Reaksi dengan rasio bahan baku H <sub>2</sub> /CO = 1	Produk
1	$3\text{H}_2 + 3\text{CO} \rightarrow \text{CH}_3\text{OCH}_3 + \text{CO}_2$	Dimetil eter
2	$2\text{H}_2 + 2\text{CO} \rightarrow \text{CH}_3\text{COOH}$	Asam asetat
3	$2 \text{R} \text{---} \text{C}=\text{O} + 2\text{H}_2 + 2\text{CO} \rightarrow \text{R} \text{---} \text{CH}_2 \text{---} \text{C}(=\text{O})\text{---} \text{CH}_3 + \text{R} \text{---} \text{CH}_2 \text{---} \text{C}(=\text{O})\text{---} \text{H}$	Aldehid dan alkohol via sintesis oxo-alkohol

(Sumber: Balasubramanian dkk., 2018)

# Battery dan H<sub>2</sub> untuk Transportasi



## Ragam lintasan:

Crude → BBM (base case)

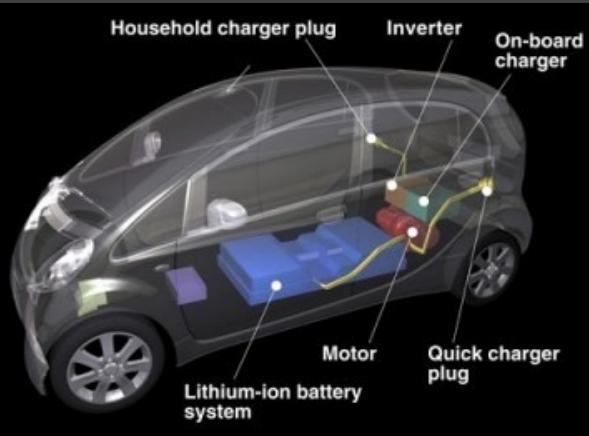
Natural gas → Listrik → Battery

Wind → Listrik → Battery

Natural gas (SMR, DRM) → Hidrogen

Natural gas → Listrik → Elektrolisis → Hidrogen

Solar PV → Listrik → Elektrolisis → Hidrogen



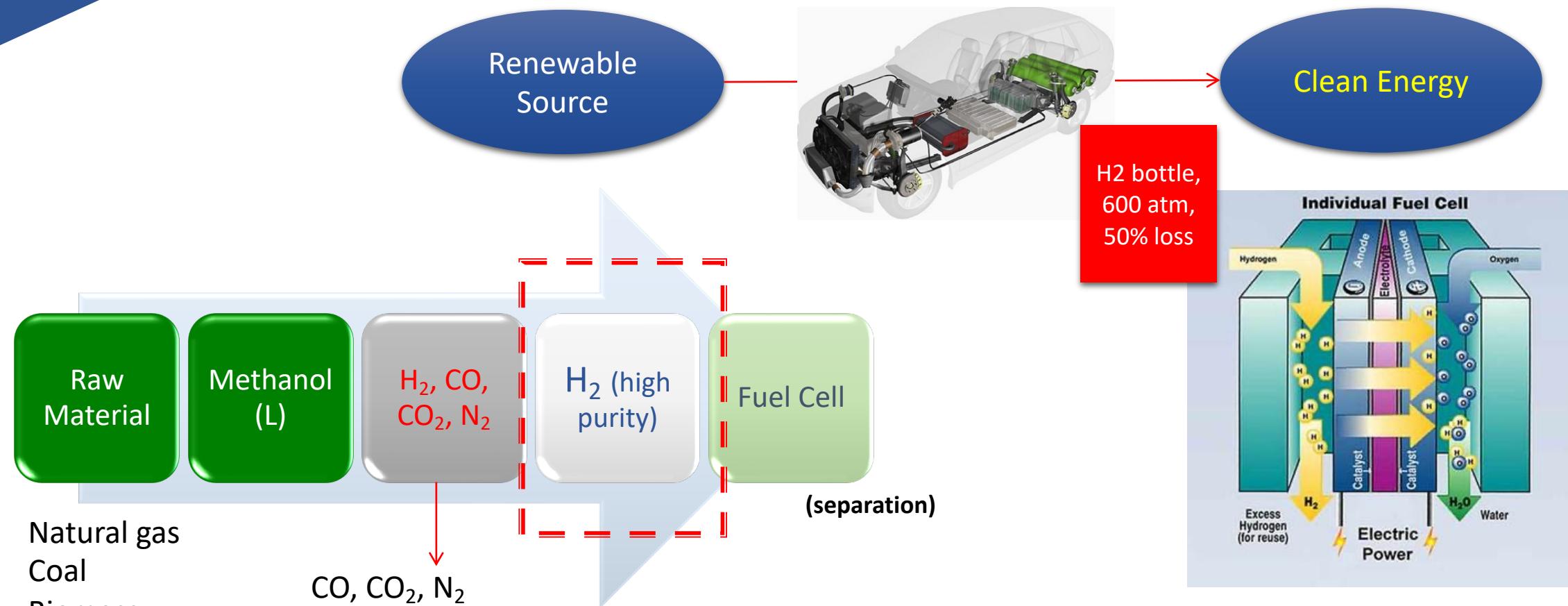
# Electric Vehicle with X - System

- **X = Battery system:**
  - Long charging time (3-5 h)
    - Tesla (super charging 120 kW, 20-75 min, specific station)
  - Limited distance (150-200 km)
  - Not practical, not flexible
- **X = Hydrogen** (liquified, > 600 atm)
  - High energy/cost
  - Safety issue/explosion

**Bagaimana dengan:**

- **X = Methanol** (liquid, atmosferik)
  - Microprocessor

# Concept of Technology Development



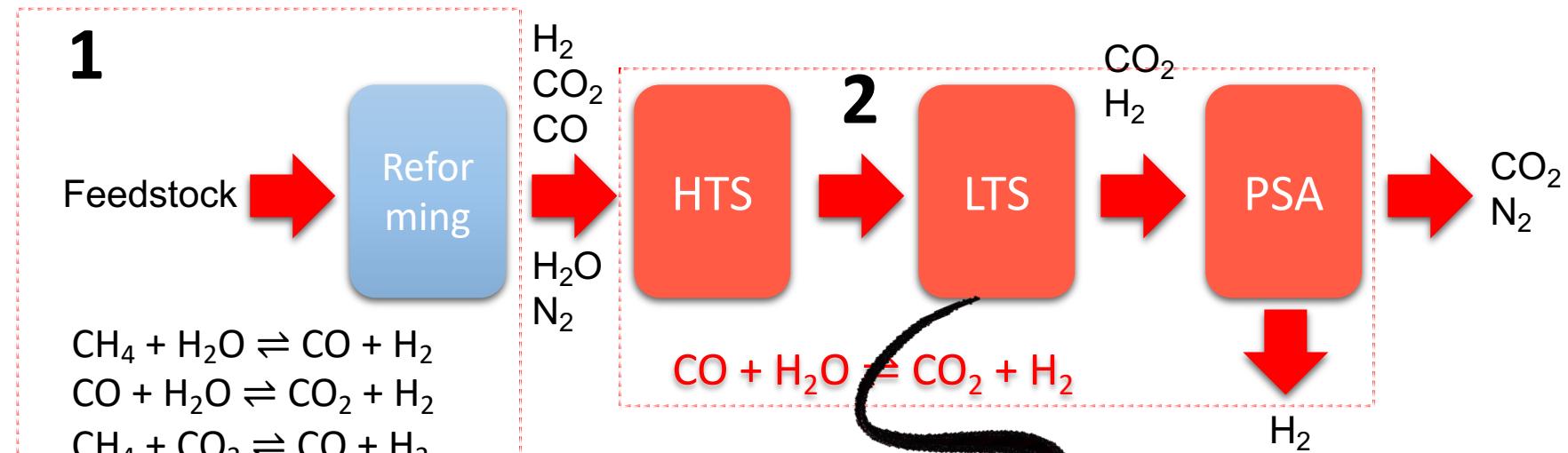
The development of an automotive industry that uses the **fuel cell** has opened a new way for utilization of hydrogen and is becoming a key process driven by spectacular advances in fuel cell technology, better known as **process intensification**.

# Process Intensification via Integration

1.  $\text{CH}_4:\text{CO}_2 = 50:50$   
•  $\text{CH}_4:\text{CO}_2 = 30:70$

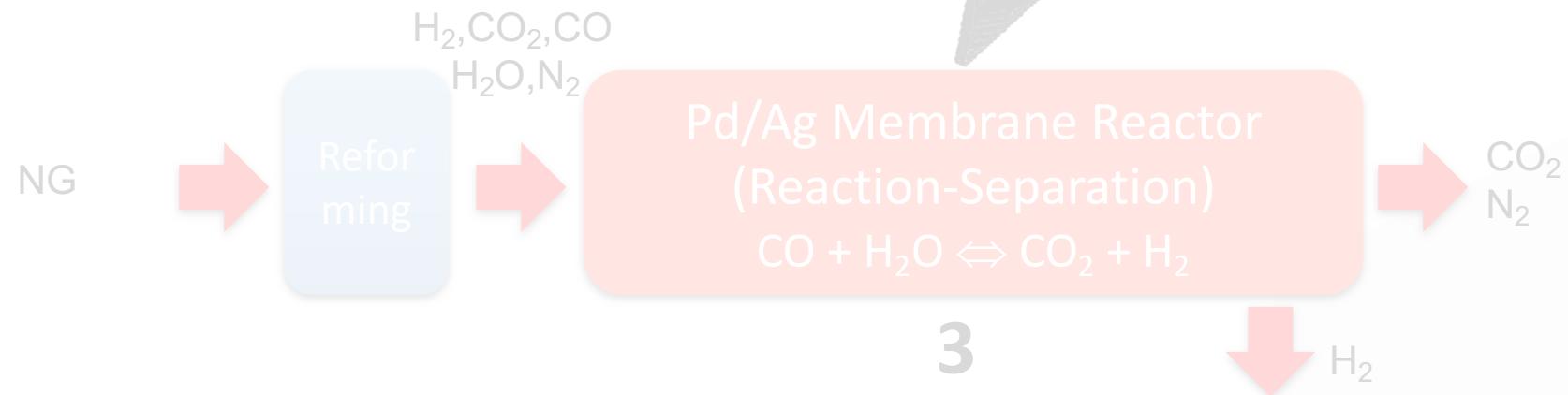
2. Catalyst:  
• Core-shell  
• Ni/MCM-41  
•  $\text{NiO}/\text{CeZrO}_2$

3. Dynamic system



HTS-LTS-PSA Integrated into Single Unit Multifunction

Feedstocks:  
- Natural gas  
- Methanol



# Application of process intensification

## Macroreactor vs Microreactor

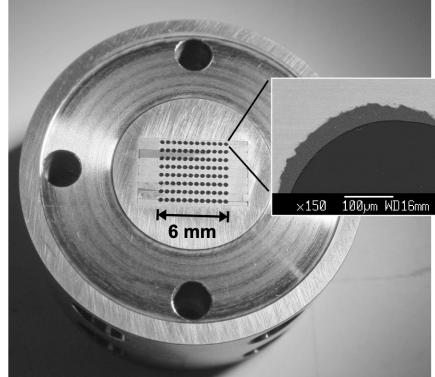


Figure 1.1: Example of a microreactor containing 96 microchannels with a diameter of 400  $\mu\text{m}$  and a length of 1.5 cm. The inlay shows a detail of a single microchannel coated with a 35  $\mu\text{m}$  thick catalyst layer.

Negligible mass and heat transfer limitations  
Fast reaction

### PI EXAMPLE FINEPHARM SECTOR - MICRO REACTOR

#### Traditional technology

Stirred Tank Reactor: the reactants are mixed in a large vessel, and the heat is removed through the jacket or a heat transfer coil (1)



#### PI technology

Micro Reactor: the reactants are mixed, and the heat is removed through thousands of micro channels, fabricated by micromachining (2) or lithography



#### Benefits

- Equipment content 3 liters versus 10  $\text{m}^3$
- 20% higher selectivity
- 20% higher material yield
- Process more reliable because continuous instead of batch
- Same capacity (1700 kg/h)

**10 m<sup>3</sup>**

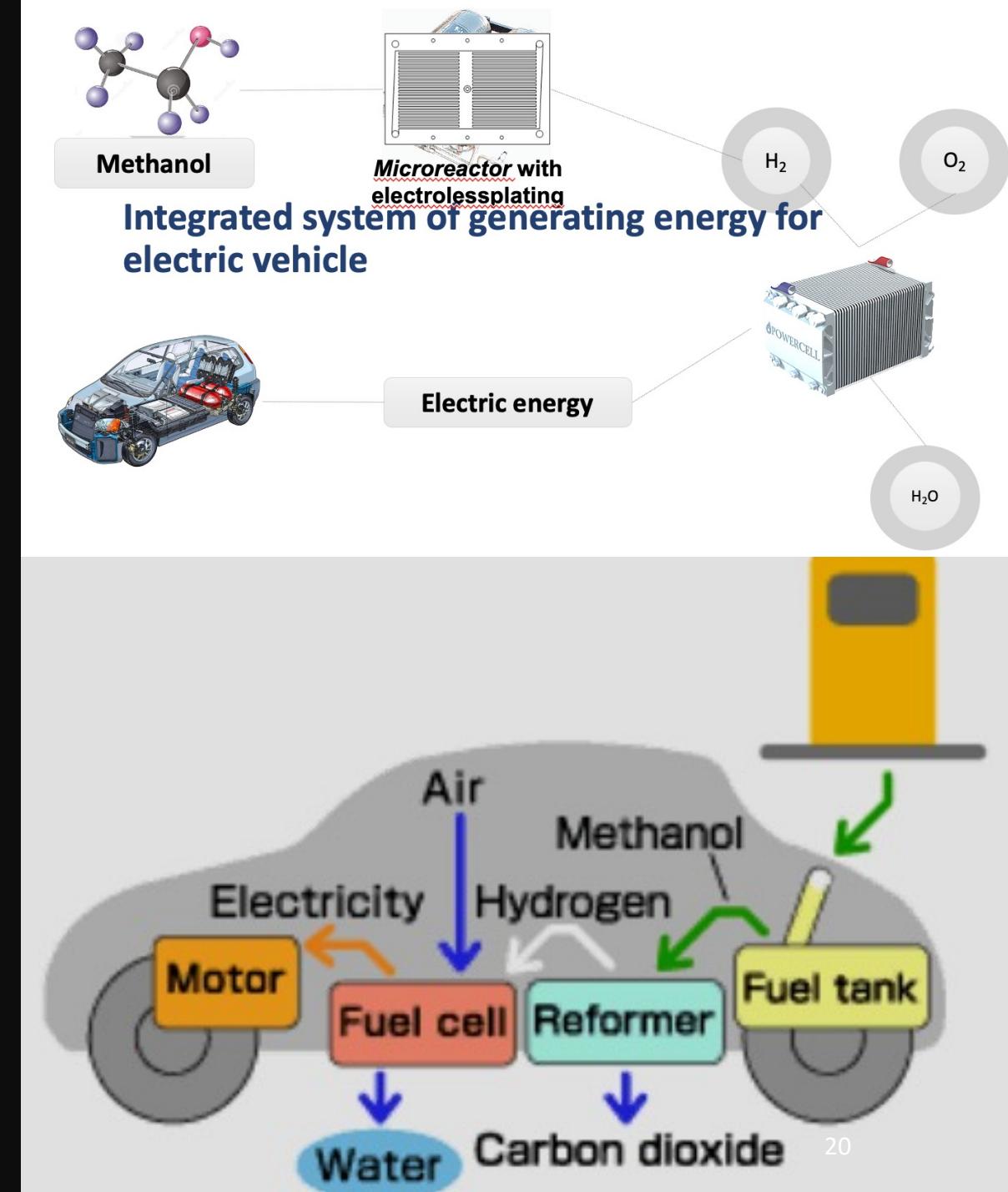
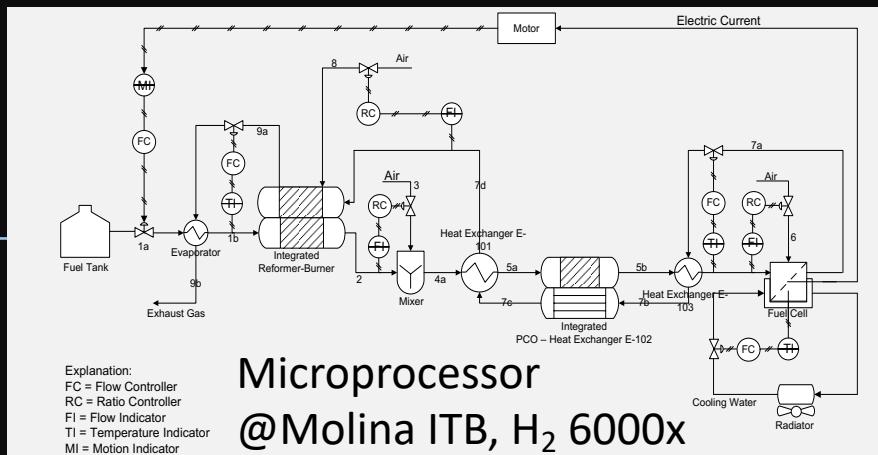
vs

**0,003 m<sup>3</sup>**

→ same capacity

# Principle of Methanol Conversion to H<sub>2</sub>

- **Advantages:**
    - Atmospheric fuel tank
    - No waiting time to refueling
    - Long trip distance
  - **Disadvantages:**
    - CO<sub>2</sub> production (exc from biomass)



# Sistem Penyedia Energi

## Energy Management System (TF)



Fuel Processor + Fuel Cell  
(TK)

Battery  
(KI+FI)

Ultracapacitor  
(EL)

Main Energy Supplier

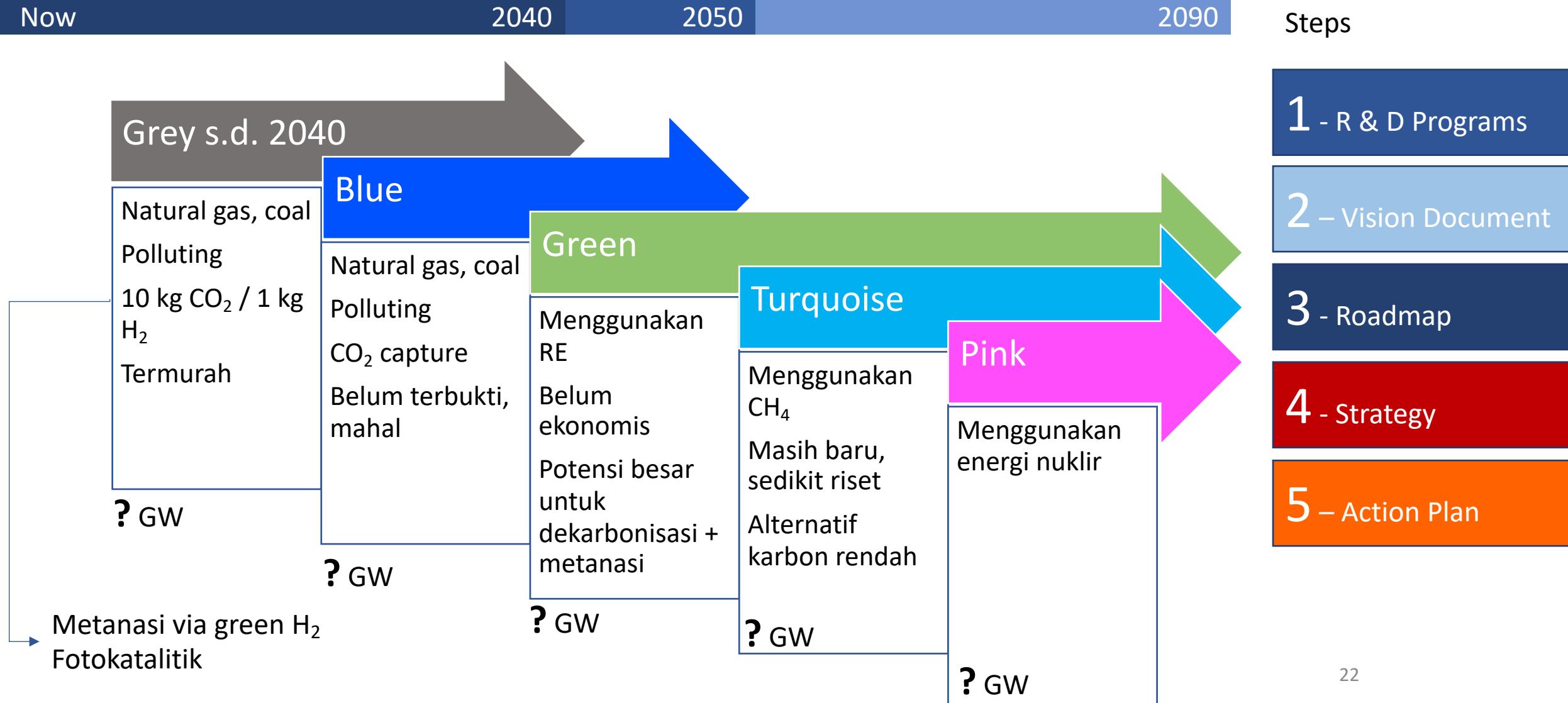
Energy Storage

Microreactor for H<sub>2</sub> production



# Konsep Peta Jalan Produksi H<sub>2</sub>

FS & Demonstration → H<sub>2</sub> refueling & Infrastructure → Enhancement → Cost Reduction → Competitive



# Penutup: Peran Intensifikasi Proses

## Pengembangan kreatif dan inovatif **Peralatan Proses**

- Microreactor: produktivitas  $H_2$  sangat tinggi
- Reforming exchanger (integrasi reaktor dan penukar panas): less energy and pollution for  $H_2$  production

## Pengembangan kreatif dan inovatif **Metode Proses**

- Tri-Reforming: optimasi produksi  $H_2$
- Utilisasi ekses energi/renewable energy: optimasi produksi  $H_2$

## Pengembangan kreatif dan inovatif **Material**

- Nanocatalyst: konversi gas alam menjadi  $H_2$
- Thin Pd-based membrane wall: untuk pemisahan  $H_2$



Terima Kasih